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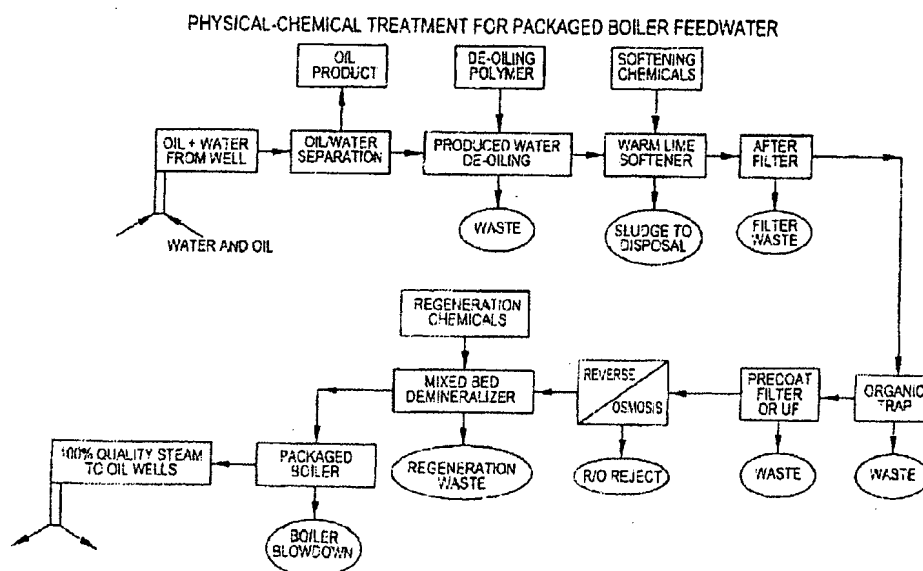
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(54) Titre : METHODE DE TRAITEMENT DES EAUX DURANT LA PRODUCTION DE PETROLE LOURD
(54) Title: WATER TREATMENT METHOD FOR HEAVY OIL PRODUCTION



(57) Abrégé/Abstract:

A method of treating produced water from heavy oil production to provide feedwater for the production of high quality steam. A produced water from heavy oil recovery operations is initially treated by first removing oil and grease to a desired level, preferably to about twenty parts per million, or less. The pH is then adjusted, normally downward and by acid addition, to release at least some carbonate alkalinity as free carbon dioxide. Preferably, all non-hydroxide alkalinity is removed, or substantially so, by introducing the feedwater into a decarbonator. In some cases, the pH may be raised (without, or subsequent to decarbonation, depending upon water chemistry) preferably by caustic addition, to maintain silica solubility in the feedwater. Next the feedwater is introduced into an evaporator, and the feedwater is evaporated to a pre-selected concentration factor to produce (1) a distillate having a small amount of residual hardness therein, and (2) a concentrate containing residual solids (dissolved solids and in some cases, suspended solids). The distillate is then cooled, and is subsequently introduced into a hardness removal step, preferably an electrodeionization (EDI) treatment unit, to remove the residual hardness from the distillate. Finally, the substantially hardness free treated water stream is sent to packaged boilers, for production of high quality steam. The hardness containing stream from EDI is recycled to the evaporator feed, for further treatment.

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WATER TREATMENT METHOD FOR HEAVY OIL PRODUCTION

ABSTRACT OF THE DISCLOSURE

A method of treating produced water from heavy oil production to provide feedwater for the production of high quality steam. A produced water from heavy oil recovery operations is initially treated by first removing oil and grease to a desired level, preferably to about twenty parts per million, or less. The pH is then adjusted, normally downward and by acid addition, to release at least some carbonate alkalinity as free carbon dioxide. Preferably, all non-hydroxide alkalinity is removed, or substantially so, by introducing the feedwater into a decarbonator. In some cases, the pH may be raised (without, or subsequent to decarbonation, depending upon water chemistry) preferably by caustic addition, to maintain silica solubility in the feedwater. Next the feedwater is introduced into an evaporator, and the feedwater is evaporated to a pre-selected concentration factor to produce (1) a distillate having a small amount of residual hardness therein, and (2) a concentrate containing residual solids (dissolved solids and in some cases, suspended solids). The distillate is then cooled, and is subsequently introduced into a hardness removal step, preferably an electrodeionization (EDI) treatment unit, to remove the residual hardness from the distillate. Finally, the substantially hardness free treated water stream is sent to packaged boilers, for production of high quality steam. The hardness containing stream from EDI is recycled to the evaporator feed, for further treatment.

CLAIMS

1. A process for producing steam for downhole injection in the recovery of heavy oil, said process comprising:
 - (a) providing an oil and water mixture gathered from an oil and water collection well;
 - 5 (b) substantially separating oil from said oil and water mixture to produce (i) an oil product, and (ii) produced water having residual oil therein;
 - (c) de-oiling said produced water to at least partially provide an evaporator feedwater, said evaporator feedwater comprising water, dissolved solutes, and dissolved gases, said dissolved solutes comprising silica;
 - 10 (d) injecting said evaporator feedwater into an evaporator; said evaporator having a plurality of heat transfer elements;
 - (e) raising the pH of said concentrated brine to maintain solubility of silica in said concentrated brine;
 - (f) distributing said concentrated brine on a first surface of at least one of said
 - 15 plurality of heat transfer elements to generate a steam vapor and further concentrating said circulating concentrated brine;
 - (g) discharging at least some of said concentrated brine as an evaporator blowdown stream;
 - (h) compressing said steam vapor to produce a compressed steam vapor;
 - 20 (i) directing said compressed steam vapor to a second surface of at least one of said plurality of heat transfer elements to condense said compressed steam vapor to form a distillate having residual solutes therein;
 - (j) collecting said distillate;

(k) introducing said distillate stream into a boiler, to produce

(i) steam,

(ii) a boiler blowdown stream, said boiler blowdown stream comprising water

5 and residual dissolved solids .

2. The process as set forth in claim 1, further comprising the step of removing said residual solutes from said distillate to produce a substantially solute free distillate stream.

10

3. The process as set forth in claim 2, wherein said residual solutes in said distillate are removed via ion exchange treatment.

4. The process as set forth in claim 2, wherein said residual solutes in said distillate
15 are removed via membrane separation, and wherein a solute containing reject stream is produced.

5. The process as set forth in claim 4, wherein said membrane separation method comprises electrodeionization, and wherein a solute containing reject stream is
20 produced.

6. The process as set forth in claim 2, wherein said residual solutes in said distillate comprise non-volatile total organic carbon constituents.

7. The process as set forth in claim 2, wherein said residual solutes in said distillate comprise hardness.

5 8. The process as set forth in claim 1, further comprising the step of adding said boiler blowdown stream to said evaporator.

9. The process as set forth in claim 1, wherein said evaporator feedwater is injected into said concentrated brine.

10

10. The process as set forth in claim 9, wherein said feedwater is injected into said concentrated brine at a location upstream of a recirculation pump.

11. The process as set forth in claim 1, further comprising the step of heating said
15 evaporator feedwater to remove at least some of said dissolved gases in said evaporator feedwater.

12. The process as set forth in claim 8, wherein said boiler blowdown is added to said evaporator feedwater prior to the step of heating said evaporator feedwater.

20

13. The process as set forth in claim 11, wherein said evaporator feedwater further comprises at least some alkalinity, further comprising the step, prior to step (d), of lowering the pH of said evaporator feedwater by the addition of acid thereto,

so as to produce at least some free carbon dioxide and to produce a pH adjusted evaporator feedwater in order to remove at least some alkalinity from said evaporator feedwater.

5 14. The process as set forth in claim 13, wherein said acid is sulfuric acid.

15. The process as set forth in claim 2, further comprising the step of cooling said distillate prior to removal of residual solutes from said distillate .

10 16. The process as set forth in claim 15, wherein said method further comprises the step of heating said substantially solute free boiler feedwater stream before introducing said boiler feedwater stream into said boiler.

15 17. The process as set forth in claim 1, or in claim 13, wherein said evaporator feedwater further comprises calcium, and wherein a slurry comprising said concentrated brine and calcium seed crystals is maintained for precipitation of said calcium to said calcium seed crystals rather than to said heat transfer surfaces of said evaporator.

20 18. The process as set forth in claim 1, wherein during the step of concentrating said circulating concentrated brine, the pH of said concentrated brine circulating in said evaporator is maintained to at least 10.5.

19. The process as set forth in claim 1, wherein during the step of concentrating said circulating concentrated brine, the pH of said concentrated brine circulating in said evaporator is maintained to between about 11 and about 12.

5

20. The process as set forth in claim 1, wherein during the step of concentrating said circulating concentrated brine, the pH of said concentrated brine circulating in said evaporator is maintained to 12 or above.

10 21. The process as set forth in claim 18, or in claim 19, or in claim 20, wherein the pH is maintained by the addition of sodium hydroxide.

22. The process as set forth in claim 1, wherein said evaporator is a falling-film evaporator.

15

23. The process as set forth in claim 1, wherein said evaporator is a forced-circulation evaporator.

24. The process as set forth in claim 22 or in claim 23, wherein at least some of
20 said plurality of heat transfer elements are tubular elements having an interior surface and an exterior surface.

25. The process as set forth in claim 24, wherein said evaporator feedwater is concentrated in the interior surface of said tubular heat transfer elements.

26. The process as set forth in claim 22 or in claim 23, wherein said evaporator
5 comprises a mechanical vapor recompression evaporator.

27. The process as set forth in claim 2, wherein said solute containing reject stream is from electrodeionization treatment, and wherein said treatment further comprises the step of returning said solute containing reject stream to said
10 evaporator feedwater prior to step (d).

28. The process as set forth in claim 1, further comprising the step of injecting said blowdown in a deep-well.

1.5 29. The process as set forth in claim 28, wherein said blowdown injected into a deep well comprises evaporator blowdown.

20 30. The process as set forth in claim 1, further comprising the step of treating said evaporator blowdown stream in a zero discharge crystallizer system.

31. The process as set forth in claim 1, further comprising the step of treating said evaporator blowdown stream in a spray dryer to dry solids in said evaporator blowdown stream.

32. The process as set forth in claim 1, further comprising, before step (d), the step of removing oil from said evaporator feedwater stream.

5 33. The process as set forth in claim 32, wherein the concentration of oil in said evaporator feedwater stream comprises less than about twenty parts per million.

34. The process as set forth in claim 1, wherein said boiler comprises a packaged boiler.

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35. The process as set forth in claim 1, wherein said boiler comprises a once-through steam generator.

15 36. The process as set forth in claim 35, wherein said once-through steam generator produces about 80% quality steam.

37. The process as set forth in claim 35, further comprising, after said once through steam generator, the step of separating steam and liquid from said 80% quality steam, to produce a steam stream having substantially 100% quality.

20

38. The process as set forth in claim 37, wherein said 100% steam quality stream is injected via injection wells to fluidize heavy oil.

39. A process for producing steam for downhole injection in the recovery of heavy oil, said process comprising:
- (a) providing an oil and water mixture gathered from an oil and water collection well;
 - (b) substantially separating oil from said oil and water mixture to provide (i) an oil
 - 5 product, and (ii) produced water having residual oil therein;
 - (c) de-oiling said produced water to at least partially provide an evaporator feedwater, said evaporator feedwater comprising water, dissolved solutes, and dissolved gases, said dissolved solutes comprising silica;
 - (d) heating said evaporator feedwater to remove at least some of said dissolved
 - 10 gases;
 - (e) injecting said evaporator feedwater into a concentrated brine in an evaporator; said evaporator having a plurality of heat transfer surfaces;
 - (f) raising the pH of said concentrated brine as necessary to maintain solubility of silica in said concentrated brine;
 - 15 (g) distributing said concentrated brine on a first surface of at least one of said plurality of heat transfer surfaces to generate a steam vapor;
 - (h) discharging at least some of said concentrated brine as an evaporator blowdown stream;
 - (i) compressing said steam vapor to produce a compressed steam vapor;
 - 20 (j) directing said compressed steam vapor to a second surface of at least one of said plurality of heat transfer surfaces to condense said compressed steam vapor to form a distillate having residual solutes therein;
 - (k) collecting said distillate;

(l) removing said residual solutes from said distillate via electrodeionization treatment or via ion exchange treatment to produce (a) a substantially solute free distillate stream and (b) a solute containing reject stream;

(m) introducing said distillate stream into a boiler, to produce

5 (i) steam,

(ii) a boiler blowdown stream, said boiler blowdown stream comprising water and residual dissolved solids,

(iii) adding said boiler blowdown stream to said evaporator feedwater prior to the step of heating said evaporator feedwater;

10 (n) injecting said steam in an injection well to produce an oil and water mixture;

(o) gathering said oil and water mixture.

WATER TREATMENT METHOD FOR HEAVY OIL PRODUCTION

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FIELD OF THE INVENTION

This invention is related to a novel process for treatment of water in operations for the recovery of oil from geological formations. More specifically, this invention relates to novel, improved techniques for the preparation of high quality water for down-hole use, and more specifically, for generation of steam for downhole use, in heavy oil recovery operations.

BACKGROUND

Water treatment is a necessary operation in heavy oil recovery operations. This is because in order to recover heavy oil from certain geologic formations, steam is required to increase the mobility of the oil in the formation. Traditionally, heavy oil recovery operations have utilized "once through" type steam generators. Such steam generators are most commonly provided in a configuration and with process parameters wherein about eighty percent (80%) quality steam is produced at about 1000 pounds per square inch (psig). The 80% quality steam (which is 80% vapor,

20% liquid, by weight) is injected via injection wells to fluidize the heavy oil. An oil/water mixture results, and the mixture is pumped to the surface. Then, the sought-after oil is separated from the water and recovered for sale.

5 The produced water stream, after separation from the oil, is further de-oiled, and is treated for reuse. Most commonly, the water is sent to the "once-through" steam generators for creation of more steam for oil recovery operations. The produced water stream is typically required to have less than about 8000 PPM TDS (as well as meeting other specific constituent requirements) for re-use. Thus, in most cases, the recovered water must be treated before it is sent to the steam generators. Normally,
10 such treatment is initially accomplished by using a warm lime softener, which removes hardness, and which removes some silica. Then, an "after-filter" is often utilized, to prevent carry-over of any precipitate or other suspended solids. For polishing, in a hardness removal step, a weak acid cation (WAC) system is often utilized to simultaneously remove hardness and the alkalinity associated with the
15 hardness. A schematic of such a typical prior art process is presented in FIG. 1.

A relatively new heavy oil recovery process, referred to as the Steam Assisted Gravity Drainage heavy oil recovery process (the "SAGD" process), ideally utilizes 100% quality steam for injection into wells (i.e., no liquid water). Initially, water utilized for generating steam in such operations can be treated much the same as in
20 the just discussed traditional heavy oil recovery operations. However, in order to produce 100% quality steam using a once-through type steam generator, a series of vapor-liquid separators are required to separate the liquid water from the steam. The

100% quality steam is then sent down the well and injected into the desired formation. A typical process flow sheet for such a process is presented in FIG. 2.

Another method for generating the required 100% quality steam involves the use of packaged boilers. Various methods are well known for producing water of
5 sufficient water to be utilized in a packaged boiler. One method which has been developed for use in heavy oil recovery operations involves de-oiling of the produced water, followed by a series of physical-chemical treatment steps. Such additional treatment steps normally include such unit operations as warm lime softening, after-filtration, organic traps, pre-coat filters or ultrafiltration, reverse osmosis, and mixed
10 bed demineralization. A typical state-of-the-art process flow scheme for utilizing packaged boilers in heavy oil recovery operations is shown in FIG. 3. Such a physical-chemical treatment system may have a high initial capital cost, and generally involves significant ongoing chemical costs. Moreover, there are many waste streams to discharge, involving a high sludge disposal cost. Further, where
15 membrane systems such as ultrafiltration or reverse osmosis are utilized, relatively frequent membrane replacement is encountered, at significant additional cost. Also, such processes can be quite labor intensive to operate and to maintain. Therefore, it is clear that the development of a simpler, more cost effective approach to produced water treatment as necessary for packaged boiler make-up water would be desirable.

20 In summary, the currently known and utilized methods for treating heavy oil field produced waters in order to generate high quality steam for down-hole are not entirely satisfactory because:

- most physical chemical treatment systems are quite extensive, are relatively difficult to maintain and require significant operator attention;
- they often require liquid-vapor separation equipment, which adds to equipment costs;
- 5 - a large quantity of unusable hot water is created and the energy from such must be recovered, as well as the water itself, in order to maintain an economic heat and material balance in plant operations;
- they require large amounts of expensive chemicals, many of which require special attention for safe handling and which present safety hazards if mishandled;
- 10 - the treatment train produces fairly substantial quantities of undesirable sludges and other waste streams;
- the disposal of waste sludges and other waste streams is increasingly difficult, due to stringent environmental and regulatory requirements.

Thus, it can be appreciated that it would be advantageous to provide a new process
15 which minimizes the production of undesirable waste streams, while minimizing the overall costs of owning and operating a heavy oil recovery plant.

SUMMARY OF THE INVENTION

My novel water treatment process can be advantageously applied to heavy oil
production operations. The method is particularly advantageous in that it minimizes the
20 generation of waste products and is otherwise superior to water treatment processes

heretofore used or proposed.

From the foregoing, it will be apparent to the reader that one important and primary aspect of the present invention resides in the provision of a novel process for the treatment of produced waters, so that such waters can be re-used in heavy oil recovery operations.

5 Another important aspect of my process is to simplify the processing procedures, which importantly, simplifies operations and improves quality control in the manufacture of high purity water for downhole applications.

Other important but more specific aspects of the invention reside in the provision of an improved water treatment process for production of high purity water for downhole use,
10 as described herein, which:

- eliminates the requirement for separation of hot liquids from generated steam;
- eliminates the generation of softener sludges;
- in conjunction with the just mentioned object, minimizes the production of undesirable waste streams;
- 15 - minimizes operation and maintenance labor requirements;
- minimizes maintenance materiel requirements;
- reduces the capital costs for water treatment equipment in heavy oil operations;
- virtually eliminates chemical additives and associated handling requirements.

Other important aspects, features, and additional advantages of my invention will

become apparent to the reader from the foregoing and from the appended claims and the ensuing detailed description, as the discussion below proceeds in conjunction with examination of the accompanying drawing.

More particularly, there is disclosed an improved water treatment process for heavy
5 oil recovery operations. This process minimizes or eliminates waste streams which must
be sent for off-site disposal of liquids or sludges and otherwise does not have the
above-discussed drawbacks common to heretofore-utilized water treatment techniques of
which I am aware. Importantly, my novel process overcomes the heretofore-encountered
shortcomings of water handling in heavy oil recovery operations. Also, it eliminates
10 undesirable multiplicity of treatment steps and unit operations seen in the more commonly
utilized alternative water treatment processes. Thus, it is believed that my novel water
treatment process will substantially simplify water treatment preparatory to steam
generation in heavy oil recovery operations. My method involves producing steam from a
selected feedwater, by first removing oil and grease to desired level, preferably to about
15 twenty parts per million, or less. Then, the pH is adjusted, normally downward and by
acid addition, to release at least some carbonate alkalinity as free carbon dioxide.
Preferably, all non-hydroxide alkalinity is removed, or substantially so, by introducing the
feedwater into a decarbonator, wherein said free carbon dioxide is substantially removed.
Next the feedwater is introduced into an evaporator and the feedwater is evaporated to a
20 pre-selected concentration factor to produce (1) a distillate having a small amount of
residual hardness therein; and (2) a concentrate containing residual solids (dissolved

solids and in some cases, suspended solids). The distillate is then cooled, and is subsequently introduced into a hardness removal step, preferably an electrodeionization (EDI) treatment unit, to remove the residual hardness from the distillate. Finally, the substantially hardness free treated water stream is sent to
5 packaged boilers, for production of high quality steam.

BRIEF DESCRIPTION OF THE DRAWING

FIG. 1 generalized process flow diagram for water treatment in prior art heavy oil
10 recovery operations.

FIG. 2 is a generalized process flow diagram for the state of the art water treatment process in steam assisted gravity drainage (SAGD) type heavy oil operations.

FIG. 3 is a generalized process flow diagram for one alternative water treatment
15 process for use in steam assisted gravity drainage (SAGD) type heavy oil operations.

FIG. 4 is a process flow diagram of my novel process for treatment of produced water in heavy oil recovery operations.

FIG. 5 shows the typical feedwater quality requirements for 1000 psig packaged
20 boilers which may be advantageously utilized in produced water heavy oil recovery operations by using my novel water treatment process.

FIG. 6 illustrates the solubility of silica as a function of pH.

FIG. 7 diagrammatically illustrates a seeded-slurry scale prevention mechanism that has been previously used at neutral or near neutral pH in the evaporation of waters containing calcium sulfate and silica.

DESCRIPTION

Since the steam assisted gravity drainage (SAGD) heavy oil recovery process utilizes 100% quality steam, it may be desirable in some instances to use a standard packaged boiler to produce the required steam, rather than to utilize a traditional once-through type steam generator. It is noteworthy in such an evaluation that packaged boilers are less expensive on a capital cost basis than once-through type oil-field steam generators. Also, package boilers are commonly utilized to produce pure steam, and thus produce only a minimal liquid blowdown stream. Unfortunately, packaged boilers require a much higher quality feed water than a once-through type steam generator. As a result, a very different approach to feedwater pretreatment (i.e., pretreatment of the produced water generated following the oil/water separation) has now been developed an alternative method for produced water treatment. My new water treatment method utilizes a mechanical vapor recompression evaporation step, followed by removal of hardness from the pure distillate produced by the evaporator. While hardness removal can be accomplished by an ion exchange system, a preferred method of hardness removal employs an electrodeionization (EDI) step. This novel combination of process treatment steps produces feedwater of sufficient quality, and in economic quantity, for use in packaged boilers in heavy oil recovery operations. A schematic of my novel process is presented in Figure 4.

Importantly, this new process method (1) eliminates many physical-chemical treatment steps commonly utilized in handling produced water, (2) results in lower capital equipment costs, (3) results in lower operating costs for steam generation, (4) eliminates the production of softener sludge, thus eliminating the need for the disposal

of the same, (5) eliminates other waste streams, thus minimizing the number of waste streams requiring disposal, (6) minimizes the materiel and labor required for maintenance, and (7) reduces the size of water de-oiling equipment in most operations.

In my process, the evaporator is designed to produce high quality distillate (typically 2-5 ppm non-volatile TDS) which can be fed directly into hardness removal equipment (i.e. the electrodeionization system), following adjustment of the distillate temperature to acceptable levels (typically by cooling to about 45°C, or lower). The water product produced by the hardness removal system is used as feedwater for the packaged boiler. Ideally, the produced waters fed to the evaporator are heated by recovering the heat transferred out of the distillate stream. A typical boiler feed water chemistry specification is presented in Figure 5. Also, in those cases where the EDI system is utilized for hardness removal, the EDI reject stream is recycled to the evaporator feed system, for reprocessing in the evaporator.

The blowdown from the evaporator is often suitable for disposal by deep well injection. Alternately, the blowdown stream can be further concentrated and/or crystallized using a crystallizing evaporator, or a crystallizer, in order to provide a zero liquid discharge type operation. This is an important advantage, since zero liquid discharge operations may be required if the geological formation is too tight to allow water disposal by deep well injection, or if regulatory requirements do not permit deep well injection.

Operating Modes for Mechanical Vapor Recompression Evaporation

Most produced waters encountered in heavy oil production are high in silica, with typical values ranging up to about 200 mg/l as SiO₂, or higher. In order to minimize the

capital cost of the mechanical vapor recompression (MVR) evaporation system, and while simultaneously providing a process design which prevents the scaling of the heat transfer surfaces with the ever-present silica, operation of the MVR evaporator at high pH, i.e., in preferably excess of about 10.5 is undertaken. More preferably, operation in
5 the range from about 11 to about 12, or higher in appropriate cases, can be used to keep the silica in aqueous solution. This is important, since silica solubility must be accounted for in the design and operation of the MVR evaporator, in order to prevent silica scaling of the heat transfer surfaces. The solubility characteristics of silica are shown in Figure 6. Since the high pH operation assures increased silica solubility, a
10 concentration factor for the MVR evaporator can be selected so that silica solubility is not exceeded. Operation at high pH also allows the use of low cost heat transfer and brine wetted surfaces, thus minimizing the capital cost of the system.

Since the calcium hardness and sulfate concentrations of many produced waters is low (typically 20-50 ppm Ca as CaCO_3), in many cases it is also possible to operate the
15 MVR evaporators below the solubility limit of calcium sulfate, with proper attention to feedwater quality and to pre-treatment processes. However, if the produced water contains an appreciable amount of calcium and sulfate, the mechanical vapor recompression evaporator can also be operated using a calcium sulfate seeded-slurry technique, even at the high pH of operation. That mode of operation can be made
20 possible by the substantial elimination of carbonate alkalinity before the feedwater is introduced into the MVR evaporator. To allow the evaporator to be constructed with low cost materials of construction, the pH can be controlled between about 11 and about 12, while operating the MVR evaporator in the seeded-slurry mode.

Operation of the MVR Evaporator in the Seeded-Slurry Mode

Prior to the initial startup of the MVR evaporator in the seeded-slurry mode, the evaporator, which is provided in a falling-film, mechanical vapor recompression configuration, the fluid contents of the unit are "seeded" by the addition of calcium sulfate (gypsum). The circulating solids within the brine slurry serve as nucleation sites for subsequent precipitation of calcium sulfate, as well as silica. Such substances both are precipitated as an entering feedwater is concentrated. Importantly, the continued concentrating process produces additional quantities of the precipitated species, and thus creates a continuing source of new "seed" material as these particles are broken up by the mechanical agitation, particularly by the action of the recirculation pump.

In order to avoid silica and calcium sulfate scale buildup in the evaporator, calcium sulfate seed crystals are continuously circulated over the wetted surfaces, i.e., the falling film evaporator tubes, as well as other wetted surfaces in the evaporator. Through control of slurry concentration, seed characteristics, and system geometry, the evaporator can operate in the otherwise scale-forming environment. The thermochemical operation within the evaporator with regard to the scale prevention mechanism is depicted in Figure 7. As the water is evaporated from the brine film inside the tubes, the remaining brine film becomes super-saturated and calcium sulfate and silica start to precipitate. The precipitating material promotes crystal growth in the slurry rather than new nucleation that would deposit on the heat-transfer surfaces; the silica crystals attach themselves to the calcium sulfate crystals. This scale prevention mechanism, called preferential precipitation, has a proven capability to promote clean heat-transfer surfaces. The details of one advantageous method for maintaining

adequate seed crystals in preferentially precipitation systems is set forth in U.S. Patent No. 4,618,429, issued October 21, 1986 to Howard R. Herrigel, the disclosure of which is incorporated into this application in full by this reference.

5 It is to be appreciated that my water treatment process for preparing boiler feedwater in heavy oil recovery operations is an appreciable improvement in the state of the art of water treatment for oil recovery operations. The process eliminates numerous of the heretofore encountered waste streams, while processing water in reliable mechanical vapor compression evaporators and electrodeionization
10 equipment. The process thus improves on currently used treatment methods by eliminating treatment chemicals, eliminating waste streams, eliminating some types of equipment and thus the complexity associated with a high number of treatment steps involving different unit operations.

 In my improved water treatment method, the control over waste streams is
15 focused on a the evaporator blowdown, which can be conveniently treated by deep well injection, or in a zero discharge system such as a crystallizer and/or spray dryer, to reduce all remaining liquids to dryness. This contrasts sharply with the prior art processes, in which sludge from a lime softener is generated, and in which waste solids are gathered at a filter unit, and in which liquid wastes are generated at an ion
20 exchange system and in the steam generators. Moreover, my waste water treatment process also reduces the chemical handling requirements associated with water treatment operations.

Although only one exemplary embodiment of this invention has been described in detail, it will be readily apparent to those skilled in the art that my novel produced waster treatment process, and the apparatus for implementing the process, may be modified from the exact embodiments provided herein, without materially departing from the novel teachings and advantages provided by this invention, and may be embodied in other specific forms without departing from the spirit or essential characteristics thereof. Therefore, the disclosures presented herein are to be considered in all respects as illustrative and not restrictive. As such, any claims are intended to cover the processes described herein, as well as legally equivalent processes. Thus, the scope of the invention is intended to include all variations described herein, whether in the specification or in the drawing, including the broad meaning and range properly afforded to the language and description set forth herein to describe such variations.

It will thus be seen that the objects set forth above, including those made apparent from the preceding description, are efficiently attained. Since certain changes may be made in carrying out the water treatment process according to the teachings herein, it is to be understood that my invention may be embodied in other specific forms without departing from the spirit or essential characteristics thereof. Many other embodiments are also feasible to attain advantageous results utilizing the principles disclosed herein. Therefore, it will be understood that the foregoing description of representative embodiments of the invention have been presented only for purposes of illustration and for providing an understanding of the invention, and it is not

intended to be exhaustive or restrictive, or to limit the invention only to the precise forms disclosed.

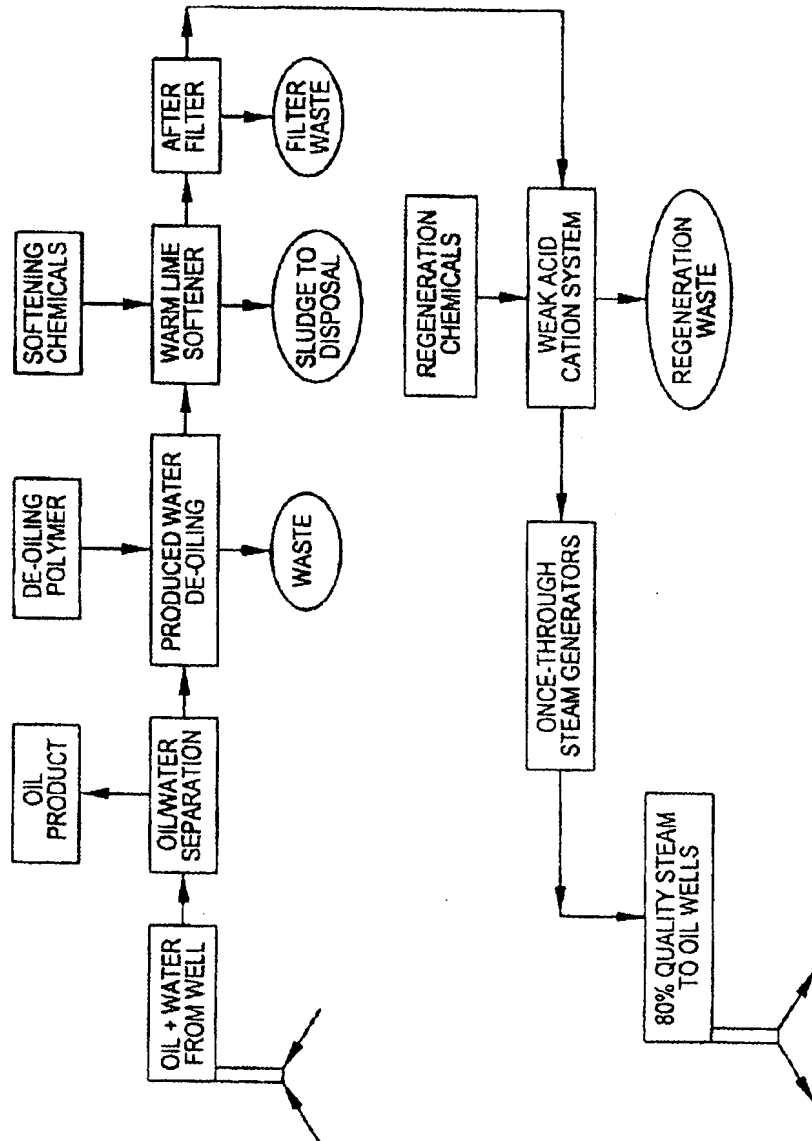
5 All of the features disclosed in this specification (including any accompanying claims, and the drawing) may be combined in any combination, except combinations where at least some of the features are mutually exclusive. Alternative features serving the same or similar purpose may replace each feature disclosed in this specification (including any accompanying claims, and the drawing), unless expressly stated otherwise. Thus, each feature disclosed is only one example of a generic series of equivalent or similar features. Further, while certain process steps are described
10 for the purpose of enabling the reader to make and use certain water treatment processes shown, such suggestions shall not serve in any way to limit the claims to the exact variation disclosed, and it is to be understood that other variations, including various treatment additives or alkalinity removal techniques, may be utilized in the practice of my method..

15 The intention is to cover all modifications, equivalents, and alternatives falling within the scope and spirit of the invention, as expressed herein above and in any appended claims. The scope of the invention, as described herein and as indicated by any appended claims, is thus intended to include variations from the embodiments provided which are nevertheless described by the broad meaning and range properly
20 afforded to the language of the claims, as explained by and in light of the terms included herein, or the equivalents thereof.

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FIG. 1
PRIOR ART

NON-SAGD HEAVY OIL RECOVERY PROCESS

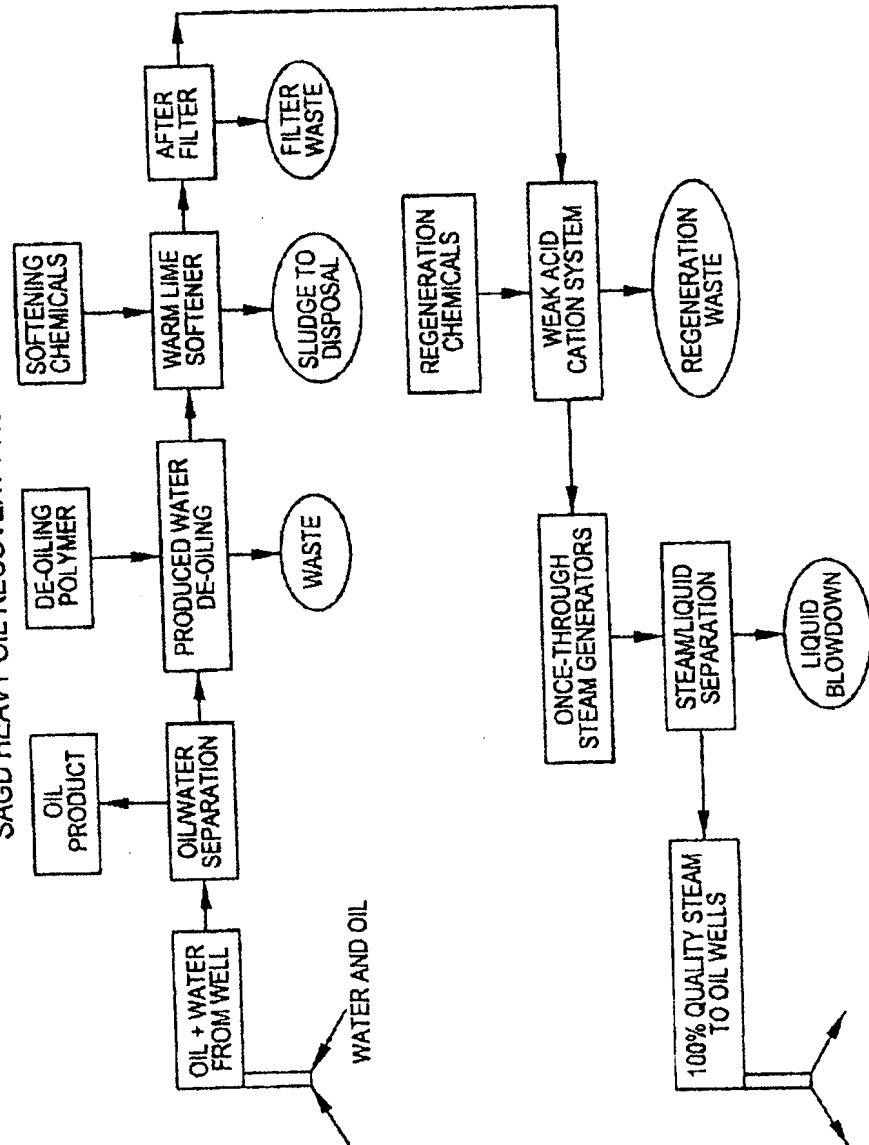


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FIG. 2
PRIOR ART

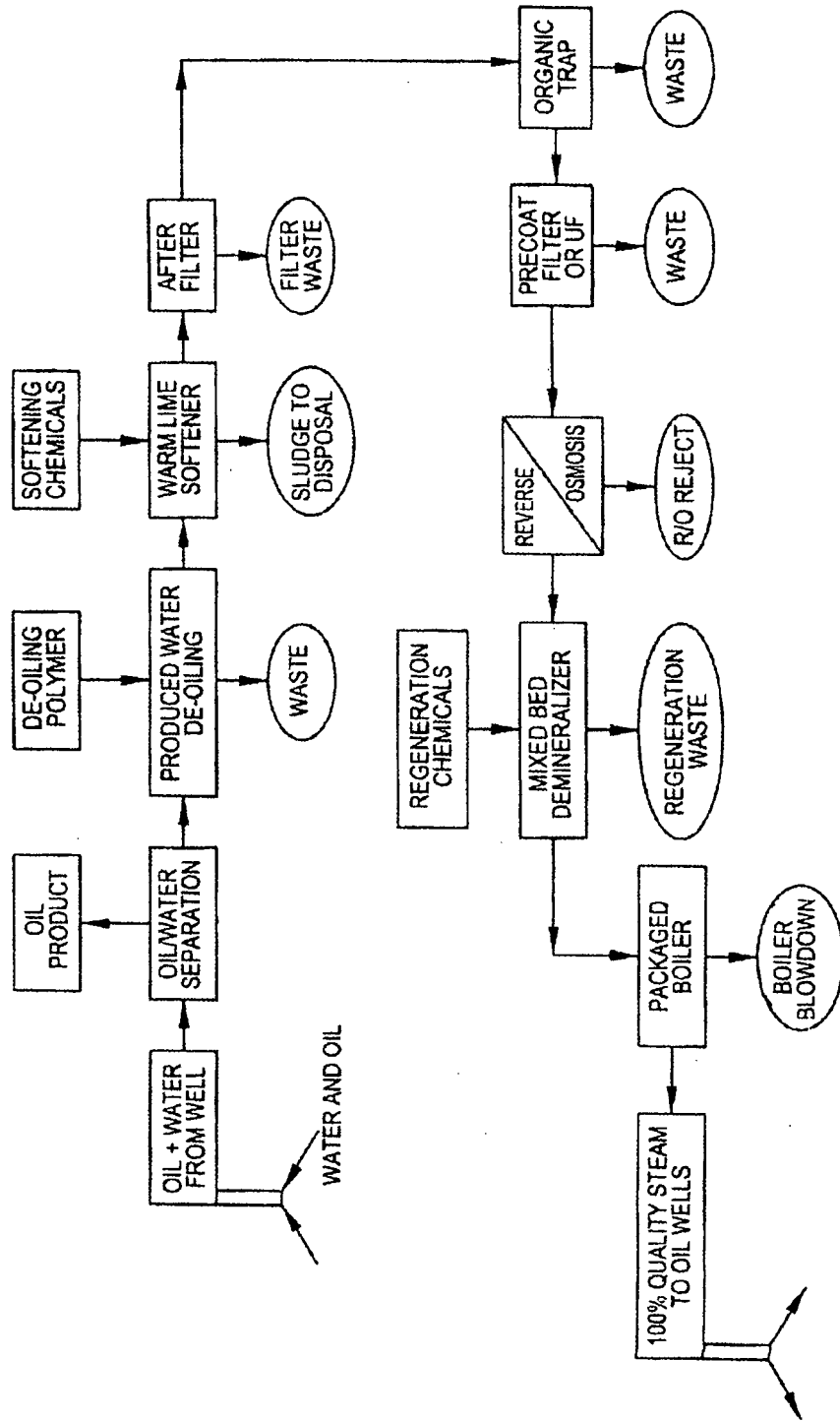
SAGD HEAVY OIL RECOVERY PROCESS



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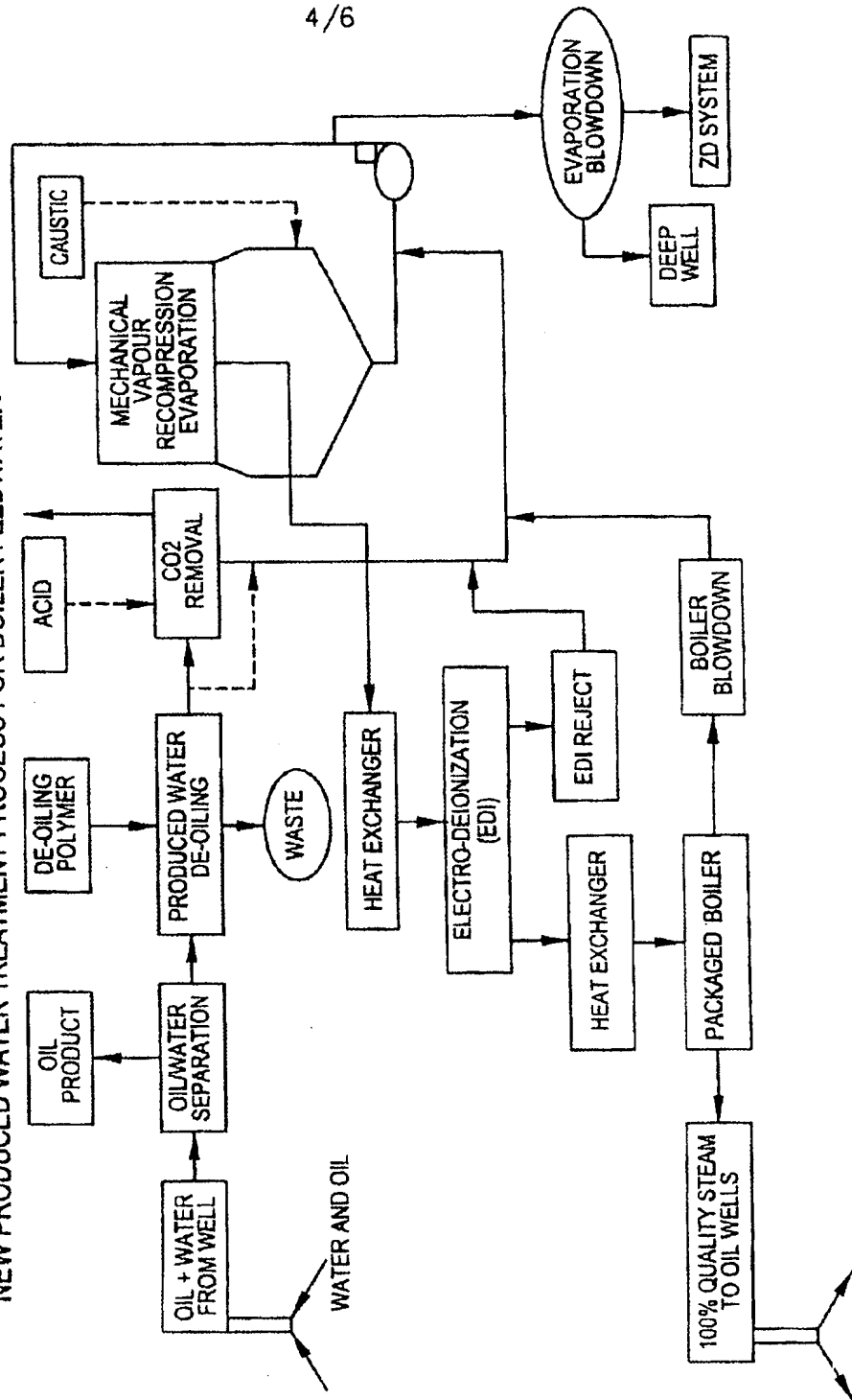
FIG. 3
PHYSICAL-CHEMICAL TREATMENT FOR PACKAGED BOILER FEEDWATER



Revised and rechecked

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FIG. 4
NEW PRODUCED WATER TREATMENT PROCESS FOR BOILER FEEDWATER



Revised Drawing

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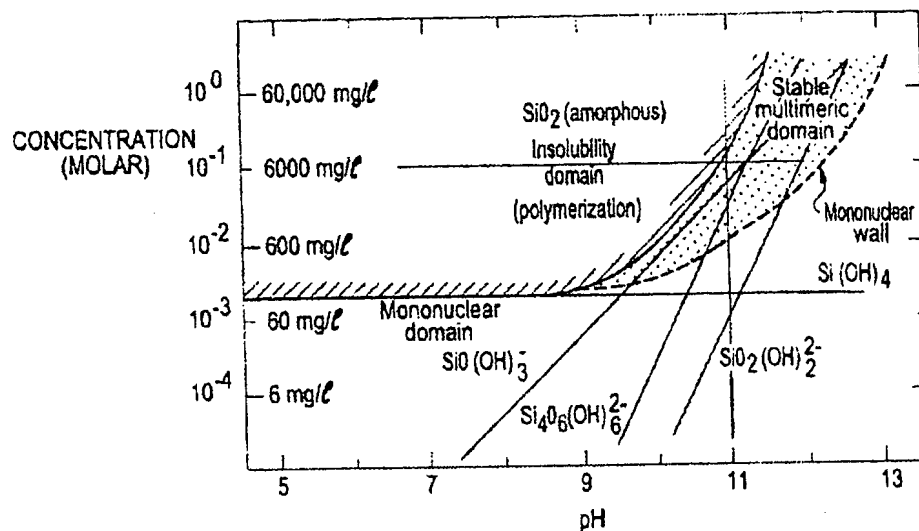
FIG. 5

TYPICAL BOILER FEEDWATER
REQUIREMENTS FOR PACKAGED BOILERS

Hardness	< 0.05 mg/l as CaCO ₃
Non-volatile TOC	< 0.20 mg/l as C
Oil & Grease	< 0.20 mg/l as substance
pH	8.8 to 9.6

FIG. 6

SILICA SOLUBILITY CHARACTERISTICS

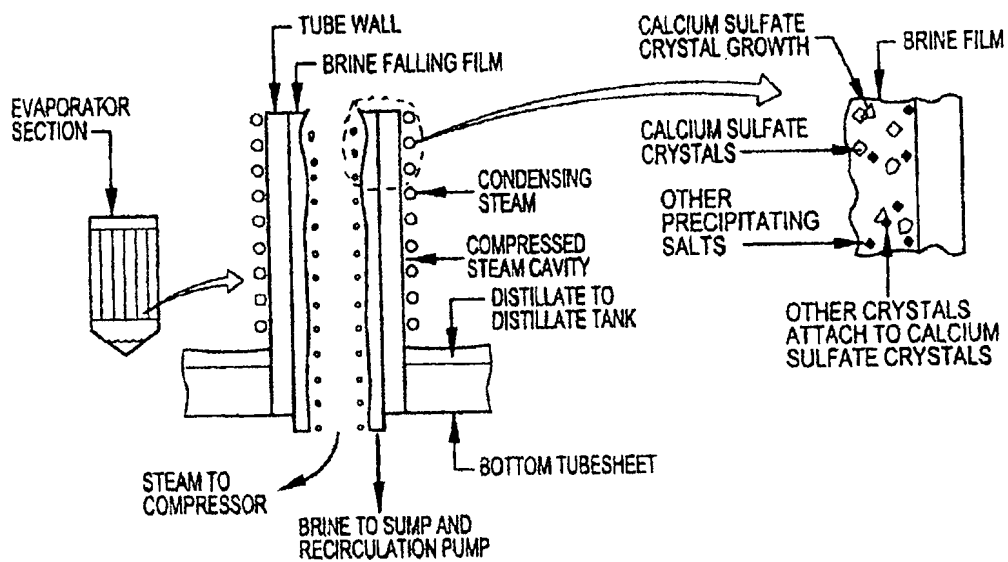


Note: Figure shows species which are in equilibrium with amorphous silica. The diagram is computed from equilibrium constants (25°C). The line surrounding the shaded area gives the maximum soluble silica. The mononuclear wall represents the lower concentration limit below which multi-nuclear silica species are not stable. In natural waters the dissolved silica is present as monomeric silicic acid.

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FIG. 7
SEEDED-SLURRY SCALE PREVENTION MECHANISM



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PHYSICAL-CHEMICAL TREATMENT FOR PACKAGED BOILER FEEDWATER

